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# 16 Saving honey

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# Problem

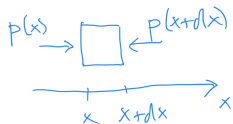
When rotating a rod coated with a viscous liquid (e.g. honey), under certain conditions the liquid will stop draining. Investigate this phenomenon.



- German site (GYPT 2022): [video](https://www.gypt.org/aufgaben/16-saving-honey.html)  
<https://www.gypt.org/aufgaben/16-saving-honey.html>
- Canadian site:  
<https://stemfellowship.org/iypt-references/problem16/>
- first analytical discussion:  
H. K. Moffatt, *Behaviour of a viscous film on the outer surface of a rotating cylinder*, J. Mec. 16, 651 (1977)
- more recent numerical analysis:  
P. L. Evans, L. W. Schwartz, and R. V. Roy, *Three-dimensional solutions for coating flow on a rotating horizontal cylinder: Theory and experiment*, Phys. Fluids 17, 072102 (2005)
- see also:  
Newtonian liquids, properties of honey  
Navier-Stokes equations, capillary length, Rayleigh-Taylor instability  
...

# Acceleration of the liquid: 1. pressure

acceleration  $\vec{f}$  if the pressure field  $p(\vec{x})$  is non-constant,  $\rho = \text{density}$



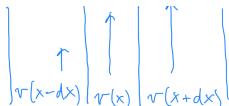
$$F = - [p(x+dx) - p(x)] \cdot S$$

$$f = \frac{F}{\rho dx \cdot S} = - \frac{p(x+dx) - p(x)}{dx}$$

$$\vec{f} = - \frac{1}{\rho} \vec{\nabla} p$$

# Acceleration of the liquid: 2. viscous forces

acceleration if the velocity field is non-constant,  $\nu =$  kinematic viscosity



internal friction:

$$\frac{\partial v}{\partial t} = \text{const.} \cdot [v(x+dx) + v(x-dx) - 2v(x)]$$

$$v(x \pm dx) = v(x) \pm \frac{\partial v}{\partial x} \cdot dx + \frac{1}{2} \frac{\partial^2 v}{\partial x^2} \cdot dx^2$$

$$\frac{\partial v}{\partial t} = \text{const.} \cdot \frac{\partial^2 v}{\partial x^2}$$

$$\boxed{\frac{\partial \vec{v}}{\partial t} = \nu \left( \frac{\partial^2}{\partial x^2} + \frac{\partial^2}{\partial y^2} + \frac{\partial^2}{\partial z^2} \right) \vec{v}}$$

# Acceleration of the liquid: 3. inertial effects

if the velocity fields depends on both time and space coordinates:

$$v(t+dt, x+dx) = v(t, x) + \frac{\partial v}{\partial t} dt + \frac{\partial v}{\partial x} dx$$

$$\frac{dv}{dt} = \frac{\partial v}{\partial t} + \frac{\partial v}{\partial x} \frac{dx}{dt}$$

$$\frac{dv}{dt} = \frac{\partial v}{\partial t} + \underbrace{\left( \frac{dx}{dt} \frac{\partial}{\partial x} + \frac{dy}{dt} \frac{\partial}{\partial y} + \frac{dz}{dt} \frac{\partial}{\partial z} \right)}_{\vec{v} \cdot \nabla} v$$

$$\boxed{\frac{d\vec{v}}{dt} = \frac{\partial \vec{v}}{\partial t} + (\vec{v} \cdot \nabla) \vec{v}}$$

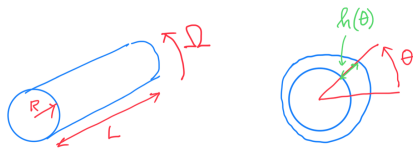
so-called **total (hydrodynamic) derivative**

# Navier-Stokes equations for honey

- Navier-Stokes equations:

$$\frac{\partial \vec{v}}{\partial t} = \vec{g} - \frac{1}{\rho} \vec{\nabla} p + \nu (\vec{\nabla} \cdot \vec{\nabla}) \vec{v} - (\vec{v} \cdot \vec{\nabla}) \vec{v}$$

- special case: fluid at rest,  $\vec{\nabla} = 0$ ; then  $\vec{g} = \frac{1}{\rho} \vec{\nabla} p$
- our case:



- 8 parameters:  $R, L, \Omega, h, g, \sigma, \rho, \nu$   
to begin with, neglect  $L$  (two-dimensional approximation)

# Dimensionless parameters

- 7 parameters:  $R, \Omega, h, g, \sigma, \rho, \nu$
- three dimensional parameters, e.g.  $R, g$ , and  $\rho$
- four dimensionless parameters, e.g.:

$$\begin{aligned}\epsilon &= \frac{\text{thickness}}{\text{radius}} = \frac{h}{R} \rightarrow h \\ W &= \frac{\text{inertia}}{\text{gravity}} = \frac{R\Omega^2}{g} \rightarrow \Omega \\ N &= \frac{\text{viscous force}}{\text{gravity}} = \frac{\nu R\Omega/h^2}{g} \rightarrow \nu \\ S &= \frac{\text{capillary length}}{\text{radius}} = \frac{\sqrt{\sigma/(\rho g)}}{R} \rightarrow \sigma\end{aligned}$$

- various regimes!



# Stationary solution of Moffatt

- assume:
  - $\epsilon \ll 1$  (thin films),  $W \ll 1$  (inertia negligible),  
 $S \ll 1$  (surface tension negligible)
- **current flows dominantly along the cylinder**, component  $u = u(r, \theta)$
- differential equation (only viscous and gravity terms):

$$\nu \frac{\partial^2 u}{\partial r^2} = g \cos \theta$$

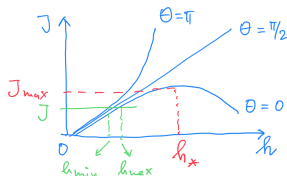
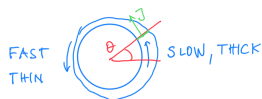
- boundary conditions for  $r = R$  (inner) and  $r = R + h(\theta)$  (outer surface):

$$u(R) = R\Omega, \quad \frac{\partial u}{\partial R} = 0$$

- solution:

$$u(r, \theta) = R\Omega + \frac{g \cos \theta}{2\nu} f(r), \quad f(r) = r^2 - 2(R + h)r + R(R + 2h)$$

# Properties of Moffatt's solution



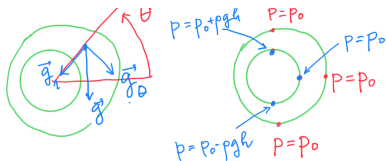
- total flow at angle  $\theta$

$$J(\theta) = \int_R^{R+h} dr u(r, \theta) = R\Omega h - \frac{gh^3}{3\nu} \cos \theta$$

- since  $J(\theta) = \text{const}$ , this defines the shape  $h = h(\theta)$
- average thickness  $h_0$  possible only for  $\Omega > \Omega_c$ , where

$$\Omega_c = \left( \frac{2\pi}{4.443} \right)^2 \frac{gh_0^2}{\nu R}$$

# Explanation of Moffatt's solution



- gravity force  $\vec{g} = \vec{g}_r + \vec{g}_\theta$
- tangential part  $g_\theta = -g \cos \theta$  **compensated by viscous forces**
- radial part  $g_r = -g \sin \theta$  **compensated by pressure**, therefore

$$\frac{1}{\rho} \frac{\partial p}{\partial r} = -g \sin \theta$$

- (strange) solution for pressure  $p(r, \theta)$ :

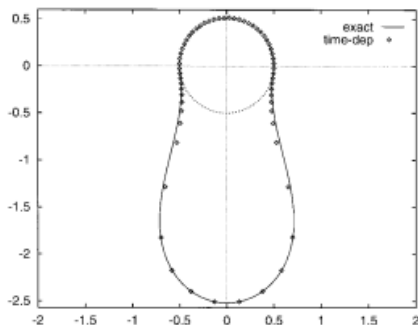
$$p(r, \theta) = p_0 + \rho g (R + h - r) \sin \theta$$

- pressure at surface:  $p(R + h, \theta) = p_0 =$  atmospheric pressure (equilibrium)

# Opposite extreme: static cylinder $\Omega = 0$

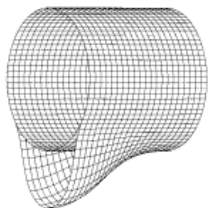
Weidner et al., J. Colloid and Interface Science 187, 243 (1997)

- surface tension can not be ignored any more
- length scale set by capillary length  $\ell_c = \sqrt{\sigma/(\rho g)}$
- two-dimensional approximation: droplet hangs under the cylinder (a ridge at  $\theta = -\pi/2$  is formed)

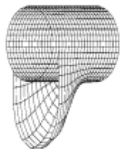


# Static cylinder $\Omega = 0$ , axial instability

Weidner et al., J. Colloid and Interface Science 187, 243 (1997)



Rc=2

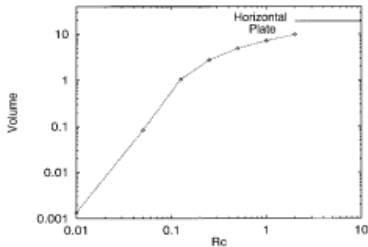


Rc=1



Rc=.5

- the ridge below the cylinder is unstable
- drops of size  $\sim l_c$  form along the cylinder
- volume of the drops (units of  $l_c^3$ ):



# Suggestions

- choose a highly viscous Newtonian liquid and a cylinder of radius  $R$ ; determine how  $h_0$  (or mass of the liquid) depends on the frequency  $\Omega$ ; compare with theory; does an optimal  $\Omega$  exist?
- try to estimate the material parameters  $\sigma$ ,  $\rho$ ,  $\nu$ ; identify the relevant dimensionless parameters
- do the results depend on the initial conditions of the experiment? how do the flow instabilities influence the results?
- try to change other parameters besides  $\Omega$  (e.g., temperature, radius  $R$ , length  $L$ , **shape of the rod**,...)